

IMPROVEMENT OF ORIENTED POLYOLEFIN PROCESSING

Field of the Invention

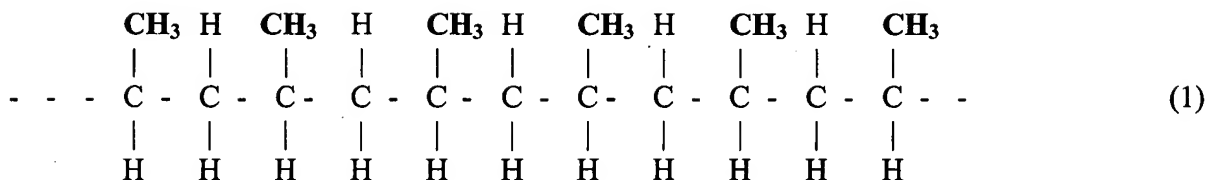
This invention relates to improved processability for the production of oriented polyolefin films, and more particularly, to polypropylene compositions which incorporate styrenic hydrocarbon resins.

Background of the Invention

Biaxial orientation of polyolefins, particularly polypropylenes, produces films which have applications in the polyolefin film business, for example snack food packaging, cigarette overwrap, electronic components wrapping, packaging tape, and shrink film. The polymers normally employed in the preparation of biaxially oriented films are isotactic homopolymers with high stereoregularity, although on some occasions the use of syndiotactic polymers has been proposed. Also suitable are co-polymers of isotactic polypropylenes with a small content of ethylene (min-random co-polymers).

Isotactic polypropylene is one of a number of crystalline polymers which can be characterized in terms of the stereoregularity of the polymer chain. Various stereo specific structural relationships denominated primarily in terms of syndiotacticity and isotacticity may be involved in the formation of stereoregular polymers of various monomers.

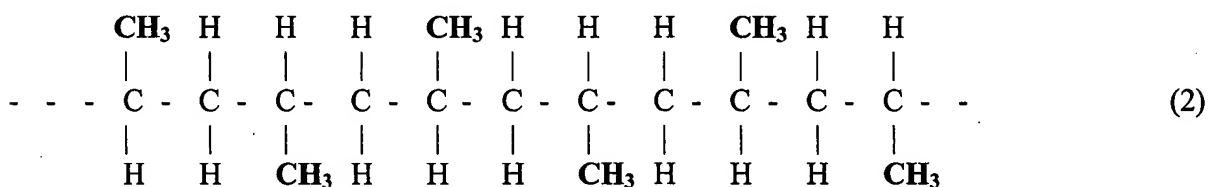
Isotactic polypropylene is conventionally used in the production of relatively thin films in which the polypropylene is heated and then extruded through dies and subject to biaxial orientation by stressing the film in both a longitudinal direction, referred to as the machine direction, and a lateral direction, sometimes referred to as the tenter direction. The structure of isotactic polypropylene is characterized in terms of the methyl group attached to the tertiary carbon atoms of the successive propylene monomer units lying on the same side of the main chain of the polymer. That is, the methyl groups are characterized as being all above or below the polymer chain. Isotactic polypropylene can be illustrated by the following structural formula:



[Bolding for emphasis only]

Stereoregular polymers, such as isotactic and syndiotactic polypropylene can be characterized in terms of the Fisher projection formula. Another way of describing the structure is through the use of NMR. Bovey's NMR nomenclature for an isotactic pentad is ...mmmm... with each "m" representing a "meso" dyad, or successive methyl groups on the same side of the plane of the polymer chain. As is know in the art, any deviation or inversion in the structure of the chain lowers the degree of isotacticity and crystallinity of the polymer.

In contrast to the isotactic structure, syndiotactic propylene polymers are those in which the methyl groups attached to the tertiary carbon atoms of successive monomeric units in the chain lie on alternate sides of the plane of the polymer. Syndiotactic polypropylene can be illustrated by the following structural formula:



[Bolding for emphasis only]

Syndiotactic polymers are semi-crystalline and, like the isotactic polymers, are insoluble in xylene. This crystallinity distinguishes both syndiotactic and isotactic polymers from an atactic polymer, which is non-crystalline and high soluble in xylene. An atactic polymer exhibits no regular order of repeating unit configurations in the polymer chain and forms essentially a

waxy product. In most cases, the preferred polymer configuration will be a predominantly isotactic or syndiotactic polymer with very little atactic polymer.

The isotactic polymers normally employed are typically prepared through the use of conventional Ziegler-Natta catalysts of the type disclosed, for example, in U.S. Patent Nos. 4,298,718 and 4,544,717, both the Myer et al. U.S. Patent No. 5,573,723 to Peiffer discloses a process for producing biaxially-oriented polypropylene film based in an isotactic polypropylene homopolymer or propylene ethylene co-polymers. Other co-polymers of propylene and alpha-olefins having from 4-8 carbon atoms also may be employed in the Peiffer process.

Catalysts employed in the polymerization of alpha-olefins may be characterized as supported catalysts or unsupported catalysts, sometimes referred to as homogeneous catalysts. Traditional supported catalysts are the so-called "conventional" Ziegler-Natta catalysts, such as titanium tetrachloride supported on an active magnesium dichloride as disclosed, for example, in the aforementioned patents to Myer et al. A supported catalyst component, as disclosed in the Myer '718 patent, includes titanium tetrachloride supported on an "active" anhydrous magnesium dihalide, such as magnesium dichloride or magnesium dibromide. The supported catalyst component in Myer '718 is employed in conjunction with a co-catalyst such and an alkylaluminum compound, for example, triethylaluminum (TEAL). The Myer '717 patent discloses a similar compound which may also incorporate an electron donor compound which may take the form of various amines, phosphenes, esters, aldehydes, and alcohols. Metallocene catalysts are often employed as unsupported or homogeneous catalysts, although, as described below, they also may be employed in supported catalyst components.

Alternative types of catalysts that produce isotactic polyolefins are disclosed in U.S. Patent Nos. 4,794,096 and 4,975,403. These patents disclose chiral, stereorigid metallocene catalysts that polymerize olefins to form isotactic polymers and are especially useful in the polymerization of highly isotactic polypropylene. As disclosed, for example, in the
5 aforementioned U.S. Patent No. 4,794,096, stereorigidity in a metallocene ligand is imparted by means of a structural bridge extending between cyclopentadienyl groups. Specifically disclosed in this patent are stereoregular hafnium metallocenes which may be characterized by the following formula:



10 In formula (3), $(C_5(R')_4)$ is a cyclopentadienyl or substituted cyclopentadienyl group, R' is independently hydrogen or a hydrocarbyl radical having 1-20 carbon atoms, and R'' is a structural bridge extending between the cyclopentadienyl rings. Q is a halogen or a hydrocarbon radical, such as an alkyl, aryl, alkenyl, alkylaryl, or arylalkyl, having 1-20 carbon atoms and p is

15 2.

The various metallocene structures as described above can be used either as so-called "neutral metallocenes" in which case an alumoxane, such as methylalumoxane, is used as a co-catalyst, or they can be employed as so-called "cationic metallocenes" which incorporate a stable non-coordinating anion and normally do not require the use of an alumoxane. For example,
20 syndiospecific cationic metallocenes are disclosed in U.S. Patent No. 5,243,002 to Razavi. As disclosed there, the metallocene cation is characterized by the cationic metallocene ligand having sterically dissimilar ring structures which are joined to a positively-charged coordinating

transition metal atom. The metallocene cation is associated with a stable non-coordinating counter-anion. Similar relationships can be established for isospecific metallocenes.

While metallocene catalysts are generally proposed for use as homogeneous catalysts, it is also known in the art to provide supported metallocene catalysts. As disclosed in U.S. Patent Nos. 4,701,432 and 4,808,561, both to Welborn, a metallocene catalyst component may be employed in the form of a supported catalyst. As described in the Welborn '432 patent, the support may be any support such as talc, an inorganic oxide, or a resinous support material such as a polyolefin. Specific inorganic oxides include silica and alumina, used alone or in combination with other inorganic oxides such as magnesia, zirconia and the like. Non-metallocene transition metal compounds, such as titanium tetrachloride, are also incorporated into the supported catalyst component. The Welborn '561 patent discloses a heterogeneous catalyst which is formed by the reaction of a metallocene and an alumoxane in combination with the support material. A catalyst system embodying both a homogenous metallocene component and a heterogeneous component, which may be a "conventional" supported Ziegler-Natta catalyst, e.g. a supported titanium tetrachloride, is disclosed in U.S. Patent No. 5,242,876 to Shamsoum et al. Various other catalyst systems involving supported metallocene catalysts are disclosed in U.S. Patent Nos. 5,308,811 to Suga et al. and 5,444,134 to Matsumoto.

Polyolefin compositions which can be oriented at variable process conditions, particularly over a range of machine direction orientation draw ratios and transverse direction orientation oven temperatures, are desirable for a number of reasons. Film manufacturers have the flexibility to vary one or more processing conditions within an acceptable range for a particular film production run. In addition, the possibility of a web break during the orientation process is lessened, resulting in lower processing line start up costs. For example, a standard

machine direction orientation draw ratio is about 5 times the original length of the polyolefin film. A standard transverse direction oven temperature is about 166° C. These processing conditions are considered standard in that the occurrence of web breaks in the film are infrequent. The ability to orient film compositions under variable conditions, for example a machine draw ratio within the range of its standard up to 9 times the original length, and a transverse direction oven temperature within the range of its standard to about 20° C less than the standard, gives manufacturers greater latitude in the production of film products. A further processing advantage is the ability to draw the film at higher line speeds thereby decreasing the manufacturing time.

Biaxially-oriented films can have a number of properties to their advantage during and after the machine processing steps. A relatively low coefficient friction is desirable, both during the biaxial orientation procedure and in the use of the ultimately-produced biaxially oriented film for end use applications. A relatively high stiffness, as indicated by the tensile modulus in both the machine direction and the transverse direction is usually advantageous. Relatively low permeabilities to gas and water are desirable. In addition, a high shrinkage factor of the processed film, while undesirable in some cases, can be advantageous in others, such as where the film is used in stretch wrapping of food products, electrical components, and the like.

Properties of the resulting film product can be dependent to a certain degree on the particular process conditions under which the polyolefin composition was manufactured. For example, a stiffer film with a higher shrinkage factor and better barrier properties would result from an orientation process incorporating a larger machine direction orientation draw ratio. Likewise, the transverse direction orientation oven temperature would affect the properties of the resulting oriented film product, particularly improving the shrinkage factor.

The physical and optical properties of films are important in the film industry and should fall within certain parameters for different film applications. The optical properties include haze, contact clarity (NAS), and gloss. Haze is a phenomena of light scattering and arises from local variations in the refractive index. Haze is defined as the relative fraction of scattered intensity
5 from the dispersed particles in all directions, being detected in a range of wide angle, to the incident light intensity. Contact clarity or NAS is a measure of contact clearness or see-through quality and is different from haze due to the direct transmittance of light. For example, some films may indeed be hazy but appear clear as the film is in contact with the contents of a package. Unlike haze, NAS clarity is distance dependent so that the thinner the film, the better
10 the contact clarity. Gloss is defined as the ratio of the reflected light intensity from the film at a specific angle of incidence light to that of a standard with the ideal smooth surface.

Summary of the Invention

In accordance with the present invention, there is provided a novel process for the production of polyolefin film using polymer compositions, particularly highly stereoregular polypropylenes or co-polymers of polypropylene with a small content of ethylene, which are blended with a resin or rosin modifier. The polymer compositions used in the present invention

5 are predominantly an isotactic polypropylene blended with a resin or rosin modifier in an amount within the range of about 1 to 30 weight percent. Preferably, the composition could contain from about 5 to 10 weight percent of a rosin or resin. Preferably, the polyolefin composition contains about 10 weight percent of the modifier. In a further aspect of the invention, there is provided a polyolefin film comprising a film layer formed of a mixture of a propylene homopolymer or a

10 co-polymer containing a small amount of ethylene, blended with a resin or rosin modifier. The resin or rosin modifier is present in the mixture in a relative amount effective to produce a biaxially oriented polyolefin film capable of being stretched up to 9 times its original length in the machine direction and stretched in the transverse direction at a temperature equal to or less than approximately 166° C. These particular homopolymer or co-polymer compositions exhibit

15 improved processability during the biaxially oriented process measured in terms of machine direction orientation draw ratios and transverse direction orientation oven temperatures. The improved processability includes fewer web breaks and drawability at higher line speeds, resulting in fewer shut downs of the processing line and decreased production time.

Brief Description of the Drawings

Figure 1 is a diagram reflecting an exemplary tenter-frame process for producing biaxially oriented polypropylene films.

Figure 2 are graphs illustrating machine direction orientation draw ratios, and the difference in transverse direction orientation oven temperatures between standard temperatures
5 given in Table 1 and the lowest temperatures reached before web breakage of biaxially oriented polypropylene films.

Detailed Description of the Invention

The biaxially oriented films of the present invention involve the use of an amount of a resin or rosin modifier in combination with an isotactic polypropylene in the production of film with enhanced processability characteristics.

5 Biaxially oriented films are characterized in terms of certain well-defined characteristics relating to their stereoregular structures and physical properties, including melt temperatures and shrinkage characteristics, as well as in relatively low coefficients of friction and relatively high tensile moduli and good barrier properties including relatively low permeation rates to oxygen and water. The biaxially oriented films of the present invention are formed using a particularly configured polyolefin polymer as described in greater detail below and by using any suitable
10 oriented film production technique, such as the conventionally-used tenter frame process.

The present invention addresses oriented films involving the combination of isotactic polypropylene with a resin or rosin modifier. The polypropylene can be polymerized with a conventional Ziegler-Natta catalyst or using a metallocene catalyst. The polymerized propylene will often include minor amounts (typically less than 1 weight percent, and more typically less
15 than 0.5 weight percent) of additives designed to enhance other physical or optical properties. Such mixtures may have, for example, one or more antioxidants present in an amount totaling no more than about 0.25 weight percent (in the tested examples below about 0.18 weight percent) and one or more acid neutralizers present in an amount totaling no more than about 0.25 weight percent (in the tested examples below about 0.05 weight percent). Although not present in the
20 tested examples, additives acting as anti-block agents may also be present, again in relatively low percentages such as no more than about 1 weight percent, more preferably no more than about 0.5 weight percent, and even more desirably no more than about 0.25 weight percent.

The polyolefins from which the film of the present invention are made are preferably isotactic homopolymers with high stereoregularity. An especially preferred polyolefin is an isotactic polypropylene with a density of from about 0.890 to 0.915 g/cc and a melt flow index of from about 1 to 5 g/10 min as determined according to ASTM D1238 (conditions 230° C and 2.16 kg). It may be made by conventional Ziegler-Natta polymerization methods. The isotactic polypropylene may also be prepared through the use of metallocene catalysts.

Alternatively, a co-polymer of propylene with up to about one (1) weight percent of another olefin, e.g. ethylene, could be used. This mini-random co-polymer of propylene and ethylene is preferably an isotactic propylene-ethylene copolymer of about 0.6 weight percent ethylene with a density of from about 0.880 to 0.910 g/cc as measured at 25° C according to ASTM D1505 and a melt flow index of from about 1 to 5 g/10 min. as determined according to ASTM D1238 (conditions 230° C and 2.16 kg). It may be made by well-known polymerization methods using a Zeigler-Natta catalyst or a metallocene catalyst.

Additives can be used in the polyolefins to affect various parameters of the biaxial oriented machine process conditions and the physical properties of the end film product. Among such additives are resin or rosin-type modifiers of the type disclosed, for example, in U.S. Patent No. 5,213,744 to Bossaert, the entire disclosure of which is incorporated herein by reference. A wide range of such additives are disclosed in Bossaert including hydrocarbon resins, such as polyturpene resins; petroleum resins; various rosin derivatives, including rosin alcohols and esters; and hydrogenated natural wood rosins. The rosin or resin modifiers disclosed in Bossaert are used in relatively high concentrations. While, as noted below, the various rosin and resin modifiers in Bossaert can be used in carrying out the present invention, preferably, they are used in amounts well below those disclosed in Bossaert. For example, Bossaert discloses preferred

resin or rosin concentrations of 22-60 weight percent, and the various examples disclose such concentrations of about 50-70 weight percent yielding the best results. Preferably the resin or rosin is hydrogenated and can be natural or synthetic. These resins can have a softening point within the range of 60° C to 180° C, preferably within the range of 136° C to 142° C. Suitable resins and rosins are the liquid and amorphous semi-solid petroleum hydrocarbons, asphalt, hydrocarbon resins such as the polyterpene resins, coal and petroleum resins, rosins, rosin derivatives, and styrene resins.

As disclosed by the Bossaert '744 patent, the polyterpene resins are a well-known class of resinous materials obtained by the polymerization or copolymerization of terpene hydrocarbons such as the alicyclic, mono-cyclic and bicyclic terpenes, and their mixtures, including careen, isomerised pinene, dipentene, terpinen, terpinolene, turpentine, a terpene cut or fraction, and various other terpenes.

Hydrogenation of the polyterpenes is accomplished by any of the conventional hydrogenation processes. Generally the hydrogenation is carried out utilizing a catalyst such as nickel, nickel on kieselguhr, copper chromite, palladium on alumina, or cobalt plus zirconia or kieselguhr. The hydrogenation is preferably carried out in the presence of a solvent such as methyl cyclohexane, toluene, p-methane, for example, utilizing pressures ranging from 500 to 10,000 psi and temperatures of 150° C to 300° C.

The petroleum resins are produced by the catalytic or thermal polymerization of a mixture of monomers derived from deep cracking petroleum whose monomers are mono- and diolefins. The petroleum resins can be hydrogenated similar to the terpene resins.

Another type of hydrocarbon resins are the polymers of unsaturated coal tar by-products such as polyindene and coumaroneidene resins. Other types include styrene resins, for example, polystyrene, styrene-olefin and styrene-diolefin copolymers, poly α -methylstyrene, and α -methylstyrene-vinyl toluene copolymer. These resins will generally have a softening point within the
5 range of 50° C to about 150° C.

The well-known types of rosins can be used in accordance with the present invention, such as wood rosin, gun rosin, tall oil rosin, and the modified rosins, such as partially or substantially completely hydrogenated rosins, dehydrogenated rosins, disproportioned rosins and polymerized rosins. In addition, rosin alcohols and heat treated rosins are suitable. These rosins
10 have softening points of at least 60° C.

Rosin esters which are suitable include the polyhydric alcohol esters of natural rosins. Hydrogenated rosins, polymerized rosins, such as the glycerol and pentaerythritol esters of wood rosin, the ethylene glycol, glycerol and pentaerythritol esters of polymerized rosin, the glycerol and pentaerythritol esters of the hydrogenated rosins.

15 Resins which can be hydrogenated are hydrocarbon resins, ketone resins, polyamide resins, colphonium, coumarone resins, terpene resins, chlorinated aliphatic or aromatic hydrocarbon resins. Typical of such resins are those manufactured by Hercules Inc. under the designation T140. These are resins of low molecular weight (MW) hydrogenated aliphatic hydrocarbon resins. The T140 resin has a weight averaged molecular weight (MW) of about 750
20 g/mol, a softening point of about 136° C to 142° C, and a glass transition temperature of about 90° C.

The polyolefin film composition of the present invention may contain a resin or rosin in an amount within the range of about 1 to about 30 weight percent. Alternatively, the composition could contain from about 5 to about 10 weight percent of a resin or rosin. Preferably, the polyolefin composition could contain about 10 weight percent of the resin or rosin. The polyolefin and resin components may be physically blended prior to melt blending or may be melt blended in a screw extruder or kneader in amounts proportionate to the relative amounts desired in the final product.

The addition of a resin or rosin to a propylene improves the processability of the polyolefin composition. The improved processability is measured in terms of machine direction orientation draw ratio and transverse direction orientation oven temperature. During biaxial orientation, the occurrence of web breaks in the film of the present invention is less frequent at standard machine direction orientation draw ratios and transverse direction orientation oven temperatures. Accordingly, the draw ratios in the machine direction can be increased and the oven temperatures of the transverse direction orientation can be lowered while processing the composition of the present invention with few web breaks. In addition, the drawability of the polyolefin composition can be accomplished at higher line speeds. The polyolefin compositions used in the present invention are desirable in that these physical and optical properties of the resulting film product are not significantly altered by the variable processing conditions.

In general, biaxially oriented film production can be of any suitable technique, such as disclosed in Canadian Patent Application No. 2,178,104 to Peiffer et al. As described in the Peiffer et al. application, the entire disclosure of which is incorporated herein by reference, the polymer or polymers used to make the film are melted and then passed through an extruder to a slot die mechanism after which it is passed over a first roller, characterized as a chill roller,

which tends to solidify the film. The film is then oriented by stressing it in a longitudinal direction, characterized as the machine direction, and in a transverse direction to arrive at a film which can be characterized in terms of orientation ratios, sometimes also referred to a stretch ratios, in both longitudinal and transverse directions. The machine direction orientation is accomplished through the use of two sequentially disposed rollers, the second or fast roller operating at a speed in relation to the slower roller corresponding to the desired orientation ratio. This may alternatively be accomplished through a series of rollers with increasing speeds, sometime with additional intermediate rollers for temperature control and other functions. After the film has been stressed in the machine direction, it is again cooled and then pre-heated and pass into a lateral stressing section, for example, a tenter frame mechanism, where it is again stressed, this time in the transverse direction. Orientation in the transverse direction is often followed by an annealing section. Subsequently, the film is then cooled and may be subjected to further treatment, such as a surface treatment (for example corona treatment or flame treatment), as described, for example, in the aforementioned Canadian Patent Application No. 2,178,104 or in U.S. Patent No. 4,692,380 to Reid, the entire disclosure of which is incorporated herein by reference. The film may also be metallized as described in U.S. Patent No. 4,692,380 to Reid. While corona and flame treatment typically occurs immediately following orientation and prior to the initial roll up, metallizing is typically performed at a separate time and location.

Turning now to Figure 1, there is shown a schematic illustration of a suitable "Tenter Frame" orientation process which may be employed in producing biaxially oriented polypropylene film in accordance with the present invention. More particularly and with reference to Figure 1, a source of molten polymer is supplied from a heated hopper 10 to an extruder 12 and from there to a slot die 14 which produces a flat, relatively thick film 16 at its

output. Film 16 is applied over a chill roller 18, and it is cooled to a suitable temperature within the range of about 30-60° C. The film is drawn off the chill roller 18 to a stretching section 20 to which the machine direction orientation occurs by means of idler rollers 22 and 23 which lead to preheat rollers 25 and 26.

5 As the film is drawn off the chill roller 18 and passed over the idler rollers, it is cooled to a temperature of about 30-60° C. In stretching the film in the machine direction, it is heated by preheat rollers 25 and 26 to an incremental temperature increase of about 60-100° C and then passed to the slow roller 30 of the longitudinal orienting mechanism. The slow roller may be operated at any suitable speed, usually about 20-40 feet per minute in this type of pilot
10 production line. The fast roller 31 is operated at a suitable speed, typically about 150 feet per minute in a pilot line, to provide a surface speed at the circumference of about 4-7 times that of the slow roller in order to orient the film in the machine direction. In a commercial production line, casting speeds may be much higher such as 20 to 60 meters per minute, with 120 to 360 meters per minute in final speeds.

15 As the oriented film is withdrawn from the fast roller, it is passed over a roller 33 at room temperature conditions. From here it is passed over tandem idler rollers 35 and 36 to a lateral stretching section 40 where the film is oriented by stretching in the transverse direction. The section 40 includes a preheat section 42 comprising a plurality of tandem heating rollers (not shown) where it is again reheated to a temperature within the range of 130-180° C. From the
20 preheat section 42 of the tenter frame, the film is passed to a stretching or draw section 44 where it is progressively stretched by means of tenter clips (not shown) which grasp the opposed sides of the film and progressively stretch it laterally until it reaches its maximum lateral dimension. Lateral stretching ratios are typically greater than machine direction stretch ratios and often

range anywhere from 5-12 times the original width. Ratios of 8-10 times are usually preferred. The concluding portion of the lateral stretching phase includes an annealing section 46, such as an oven housing, where the film is heated at a temperature within the range of 130-170° C for a suitable period of time, about 1-10 seconds. The annealing time helps control certain properties, and increased annealing is often specifically used to reduce shrinkage. The biaxially oriented film is then withdrawn from the tenter frame and passed over a chill roller 48 where it is reduced to a temperature of less than about 50° C and then applied to take-up spools on a take-up mechanism 50. From the foregoing description, it will be recognized that the initial orientation in the machine direction is carried out at a somewhat lower temperature than the orientation in the lateral dimension. For example, the film exiting the preheat rollers is stretched in the machine direction at a temperature of about 120° C. The film may be cooled to a temperature of about 50° C and thereafter heated to a temperature of about 160° C before it is subject to the progressive lateral dimension orientation in the tenter section.

The following example illustrates the unexpected advantages in the biaxial orientation processability provided by the present invention. The example also provides an illustration of the effects of the present invention on other physical and optical properties.

Example

Several compositions with varying amounts of primarily isotactic polypropylene (referred to simply hereinafter as isotactic polypropylene or "iPP"), blended with a hydrocarbon resin, were processed through a biaxially oriented polypropylene film making process using a tenter frame system while measuring their processing properties. The hydrocarbon resin was melt blended with the polymer in a screw extruder.

The trial was conducted in a sixty inch continuous pilot tenter line capable of 76.2 meters per minute output. Biaxial orientation of flat films was carried out in two sequential steps. The casted sheet chilled on a rotating cold steel roll was first stretched longitudinally (in the machine direction or "MD") in the tangential gap between sets of rolls rotating at different speeds.

- 5 Subsequently, the film was stretched transversely (in the transverse direction or "TD") in a tenter frame in which the edges of the film were gripped by a series of clips and diverged in TD.

Three samples of polyolefin compositions were evaluated for orientation processability by increasing the machine direction orientation (MDO) stretch ratio and lowering the transverse direction orientation (TDO) oven temperature from their standards until web breaks occurred.

- 10 Standard MDO draw ratio was 5 times the original length of the film in one stage while the TDO draw ratio was consistently 9 times the original width. The MDO stretch experiments were performed at a constant film thickness of approximately 0.7 mil. By varying the cast/chill roll speed while keeping the final film speed at 150 ft./min. Temperature settings are listed in Table 1 below:

15

TABLE 1
Temperature Settings for Standard Conditions

Temp	Melt	Cast Roll	Chill Roll	MDO			TDO		
				Cond	Stretch	Anneal	Cond	Stretch	Anneal
°C	235	54	43	116	121	138	168	166	160
°F	455	130	110	240	250	280	335	330	320

- This process was used to evaluate the processability of the three biaxially oriented polypropylene film samples with various hydrocarbon resin fractions. The first sample was a homopolymer having a density of about 0.91 g/cm³, xylene solubles of about 3.0 weight percent,
- 20

and a melt flow index of about 1.8 g/10 min. as determined according to ASTM D1238 (conditions 230° C and 2.16 kg). Additives in the polypropylene of the first sample included about 0.12 weight percent of Irganox 1010 and about 0.06 weight percent of Irganox 1076 (antioxidants), and about 0.05 weight percent of calcium stearate (an acid neutralizer).

5 The second sample was higher crystallinity polypropylene having a density of about 0.91 g/cm³, xylene solubles in the range of about 1.5 to 2.0 weight percent, and a melt flow index in the range of about 2.0 to 2.5 g/10 min as determined according to ASTM D1238 (conditions 230° C and 2.16 kg). Additives contained in the second sample were the same and in the same amount as those in the first sample.

10 The third sample was a blend of about 90 weight percent of higher crystallinity polypropylene and about 10 weight percent of a low molecular weight hydrogenated hydrocarbon resin. The blend has a density of about 0.92 g/cm³ and a melt flow index of about 3.3 g/10 min as determined according to ASTM D1238 (conditions 230° C and 2.16 kg). Again, additives in the polypropylene of the third sample were the same as those in the previous
15 samples. The resin contained in the third sample has a weight averaged molecular weight (MW) of 750 g/mol, a softening point of 140° C, and a glass transition temperature of 90° C. More specifically, the modifier is the resin marketed by Hercules Inc. under the designation T140.

Figure 2 compares processability of the three polyolefin compositions of biaxially oriented films in terms of the maximum draw ratio in MDO and the difference in TDO oven
20 temperatures between the standard temperatures of Table 1 and the lowest temperatures reached before web breaks occurred.

As illustrated in Figure 2, the polyolefin composition containing about 10 weight percent of the hydrocarbon resin significantly increased the drawability in MDO and lowered the TDO oven temperatures. A MDO draw ratio of about 9 times the original length and a TDO oven temperature of about 20° C less than the standard condition of about 166° C in Table 1 were
5 achieved by the composition without the occurrence of web breaks.

Table 2 compares the film properties in opticals, stiffness, friction, and shrinkage, as well as the barrier properties of moisture vapor and oxygen transmission rates.

TABLE 2
End Product Film Properties

	ASTM Standards	Sample 1	Sample 2	Sample 3
Gauge, micron	--	17	18	17
Treat, dynes/cm	--	44	42	56
Haze, %	D1003	0.3	0.3	0.6
NAS, %	--	70	60	72
Gross, %	D2457	99	98	99
Tensile MD, MPa	D882	126	150	107
Tensile TD, MPa	D882	300	322	259
Elongation MD, %	D882	142	157	106
Elongation TD, %	D882	53	45	39
Secant Mod MD, GPa	D882	1.33	1.56	1.58
Secant Mod TD, GPa	D882	1.78	2.82	2.19
Shrink MD, %	1204	7.1	5.4	5.1
Shrink TD, %	1204	9.7	10.2	4.8
COF T/T, Static	D1894	0.84	0.76	0.54
COF T/T, Kinetic	D1894	0.74	0.68	0.74
MVTR, gm/m ² /day	D1249-90 (at 85°F; 100% RH)	3.410	2.945	2.015
OTR, cc/m ² /day	D3985 (at 73°F; 0% RH)	2635	2186	1426

As shown in Table 2, the optical and physical properties of the film containing the resin modifier are fairly standard properties to homopolymers as indicated by its similarity with the properties of the 100 weight percent polypropylene films. Accordingly, the addition of the resin modifier improved the processability of the homopolymers in terms of increased MDO draw ratio and lowered TDO oven temperatures, but does not alter significantly their properties.

The optical properties of haze, contact clarity (NAS) and gloss for the three film samples are relatively similar. The stiffness, measured by tensile strength, elongation and secant modulus, does not vary significantly.

The moisture vapor and oxygen transmission rates of the film containing the resin
5 modifier are significantly reduced, and thus improved over the pure homopolymers.